

1 **An experimental investigation on the substitution of R134A with**
2 **HFO1234YF in the domestic refrigerators**

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4 Ciro Aprea^a, Adriana Greco^b, Angelo Maiorino^{a,†}

5 ^a Department of Industrial Engineering, University of Salerno,
6 Via Giovanni Paolo II 132, 84084, Fisciano (SA), Italy

7 ^b Department of Industrial Engineering, University of Naples Federico II,
8 P.le Tecchio 80, 80125, Napoli, Italy

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10 [†] Corresponding author: Tel. +39 089 964002; Fax +39 089 964037;
11 email: amaiorino@unisa.it

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15 **Abstract**

16 *The latest international regulations on the reduction of greenhouse gases are*
17 *strongly redesigning the scenario of use of refrigerants, gradually eliminating the*
18 *possibility of employing the HFCs. Among all sectors of refrigeration, one of the*
19 *most affected by these restrictions is the domestic refrigeration. Although for it*
20 *have been suggested some solutions, such as the construction of household*
21 *refrigerator operating with the hydrocarbons, there remains the need to find a*
22 *substitute for R134a. In particular, the substitution may involve both existing*
23 *machines and already in operation, which can not be loaded with hydrocarbons,*
24 *and new devices. With the aim of finding a simple implementation solution, in the*
25 *present work, it is reported an experimental investigation carried out on a*
26 *domestic refrigerator designed and built to operate with R134A and for which a*
27 *drop-in with HFO1234YF has been realised. The experimentation has been*
28 *addressed so as to highlight the behaviour of the system as a result of the drop-in,*
29 *with a particular interest in the energy performance variation.*

30
31 Keywords: R134A; HFO1234YF; drop-in; domestic refrigerator; energy
32 saving; environmental impact

1	Nomenclature		
2	E	electrical energy consumptions	[Wh]
3	GWP	global warming potential	
4	h	enthalpy	[kJ kg ⁻¹]
5	HOC	heat of combustion	[MJ kg ⁻¹]
6	LFL	lower flammability limit	[% vol]
7	P	electrical power absorbed	[W]
8	p	pressure of the refrigerant	[bar]
9	OEL	occupational exposure limit	[PPMv]
10	S _{cab}	external surface of the cabinet	[m ²]
11	U	Thermal trasmittance of the walls	[Wm ⁻² K ⁻¹]
12	V _{in,cab}	internal volume of the cabinet	[m ³]
13	t	time	[s]
14	T	temperature	[°C]
15			
16	Greek Symbols		
17	δ	duty cycle	[%]
18			
19	Subscripts		
20	1y	along 1 year	
21	air	of air	
22	c	cabinet	
23	cond	condensation, condenser	
24	dis	discharge of the compressor	
25	ev	evaporator	
26	f	at freezer	
27	H24	along 1-day	
28	i	at inlet	
29	o	at outlet	
30	pd	during the pull-down test	
31	r	at refrigerator	
32	ref	of refrigerant	
33	suc	suction of the compressor	
34	sor	sorround	
35	ON	phase of working of the compressor	
36	OFF	phase of stop of the compressor	
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1 **1. Introduction**

2 The focus in reducing the global warming of our planet has led to consider
3 the synthetic refrigerants with more uncertainty. Whilst in recent decades there
4 has been considerable interest in rediscovering the use of natural fluids [1–6], in
5 most real applications still dominate the synthetic fluids such as the hydro-
6 fluoro-carbon (HFC). These fluids, greeted with a considerable enthusiasm at the
7 end of the last century for their zero ODP, now are considered particularly
8 damaging to the environment because of their GWP, which is equal to more than
9 1000 times that of carbon dioxide. In recent years, there have been some
10 legislative procedures restricting the use of HFCs. In Europe, the phase-out of
11 HFCs has already been scheduled and initiated on 1st of January, 2015[7],
12 banning the use of fluids with a GWP greater than 150 for the household
13 refrigerators. Similar measures have been adopted in Japan while they are being
14 studied in Canada, the United States and Mexico, where it is expected the
15 beginning of the phase-out of HFCs as of January 1 of 2019[8]. Therefore, an
16 impending world needing to replace these refrigerants with others having low
17 GWP exists. In some field, such as domestic refrigeration, it has already been
18 proposed to replace R134a, reference fluid used from the 90s[9], with isobutane
19 (R600a). However, although this solution has already been accepted by the
20 European market, it involves some technical difficulties related to the high
21 flammability of R600a. While the reduced amount of charge present in a
22 domestic refrigerator for the European market is not of particular concern, the
23 manufacturers of the household refrigerator had to redesign some areas of their
24 production plant (i.e. warehouse storage of refrigerant, and charging stations),
25 causing massive investments for the companies involved. Of no lesser
26 importance is the adoption of specific components (i.e. the compressors) able to
27 operate with HCs. Also, as evidenced by Bansal et al. [10] the use of R600a may
28 have high barriers to the American market (US market) because of more
29 stringent standards for fire prevention (UL Standard 250), as well as other
30 markets might be reluctant to such a solution. An alternative solution has been
31 put forward with the introduction into the market of the fourth generation
32 refrigerants: the hydro-fluoro-olefins (HFO) characterised by GWP values less
33 than 10, such as HFO1234ZE and HFO1234yf. To date such fluids have been
34 widely investigated under different points of view:

- 35 1. Flammability and toxicity[11–14]
- 36 2. Heat transfer properties and Thermodynamic[15–23]
- 37 3. Energy performances [22,24–32]
- 38 4. Solubility with POE, PAG, and Mineral oil [33–36].

39 Based on the works just mentioned, it is clear that the majority of experimental
40 investigations, aimed at evaluating the energy performances achievable with
41 HFO, was produced using plants for air conditioning, mobile air-conditioning,
42 and commercial refrigeration. According to [10,37], it is evident the absence of
43 experimental investigation ended to validate the possibility of replacing R134a

1 with HFOs in domestic refrigerators, and at the same time, it highlights the need
 2 to investigate in that direction. In this regard, this article presents the
 3 experimental analysis of HFO1234YF (Tab. 1 and Fig. 1) as a drop-in
 4 replacement for R134A in a frost-free domestic refrigerator.
 5

	HFO1234YF	R134A
Chemical formula or composition [%wt]	CH ₂ =CFCF ₃	CH ₂ FCF ₃
Molecular weight [g mol ⁻¹]	114.04	102.03
Normal boiling point [°C]	-29.5	-26.1
Critical temperature [°C]	94.7	101.1
Latent heat at -30°C [kJ kg ⁻¹]	180.51	219.5
Latent heat at +40°C [kJ kg ⁻¹]	132.27	163.0
Specific volume at -30°C [m ³ kg ⁻¹]	0.1708	0.2259
GWP _{100 years}	4	1370
Safety Group (Ashrae stand 34-2010)	A2 (A2L)	A1
OEL [PPMv]	400	1000
LFL [% vol]	6.2	None
HOC [MJ kg ⁻¹]	n.a.	4.2

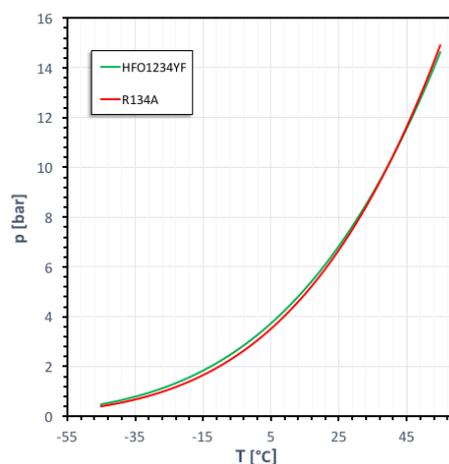
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8 *Tab. 1. Physical, environmental and safety characteristics of the considered*
 9 *refrigerants [38]*

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11 2. Investigation

12 With the aim to analyse the feasibility of replacing R134a with HFO1234YF in
 13 a domestic refrigerator, it has been examined a recently constructed commercial
 14 device.



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18 *Fig. 1 Saturation pressure for R134A and HFO1234YF*

19 As a starting point of the investigation, it has been carried out a
 characterization of the fridge as well as it was built regarding energy

1 consumptions and pull-down time. Successively, the refrigerator has been
 2 subjected to the "drop-in" of R134a with HFO1234YF. Finally, it has proceeded to
 3 a new characterization of the apparatus in agreement with what will be
 4 described below. Fig. 1 shows the saturation pressures as a function of
 5 temperature for the two refrigerants under investigation.

6 7 **2.1. Experimental facility**

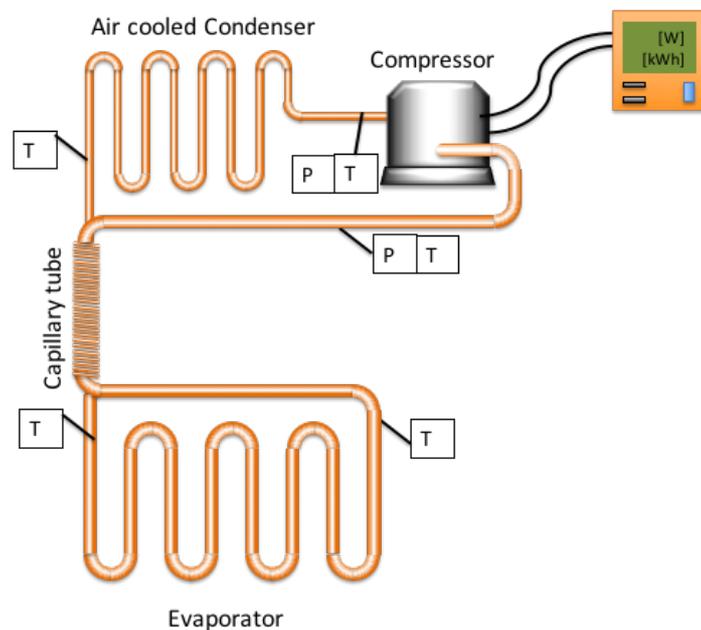
8 The plant used for the experimental investigation is a frost-free domestic
 9 refrigerator having a charge of R134A equal to 100 g, as defined by the
 10 manufacturer. The refrigerator cabinet is divided into two separate
 11 compartments: a three-star freezer (hereto referred to as freezer), and a fresh
 12 food storage (hereto referred to as refrigerator). In Tab. 2 are given the
 13 additional features of the two compartments. In particular, it shows the value of
 14 U obtained experimentally using a thermal conductivity meter.

	Dimension	Freezer compartment	Refrigerator compartment
$V_{in,cab}$	[m ³]	0.131	0.342
S_{cab}	[m ²]	2.20	3.30
U	[Wm ⁻² K ⁻¹]	0.369 ±2.4%	0.369±2.4%
U*S _{cab}	[WK ⁻¹]	0.81	1.22
Position	[-]	Upper side	Lower side

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17 *Tab.2 Characteristics of the compartments.*

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19 For both compartments there is a single cooling circuit (Fig. 2) composed of a
 20 hermetic reciprocating compressor, a forced air cooled condenser, a capillary
 21 tube and an evaporator operating in forced convection. The evaporator is
 22 entirely inserted into the freezer compartment, while an air distribution system,
 23 comprising an air delivery duct and an air suction duct, connects the refrigerator
 24 to the freezer. In this way, in the freezer compartment, it is established a cold air
 25 circulation that allows reaching a low temperature (-18°C). Also, a portion of air
 26 coming from the freezer reaches the refrigerator compartment and allows for
 27 keeping the air temperature to an intermediate level (+5°C). A damper valve,
 28 moved using a thermostatic mechanical drive, controls the amount of air
 29 delivered to the refrigerator compartment. The user desired temperature levels
 30 be selected using two regulators: a digital type connected to the freezer, and a
 31 mechanical type plugged into the refrigerator compartment. The first directly
 32 controls the operation of the compressor, while the second acts on the
 33 mechanical damper adjustment. The capillary tube is wrapped for a good part of
 34 its length (>90%) around the suction pipe of the compressor. In this way, during
 35 the lamination, the refrigerant becomes cool thanks to the refrigerant leaving the

1 evaporator. As a consequence, the enthalpy variation of the fluid at evaporator
2 increases, while the refrigerant leaving the evaporator undergoes an additional
3 overheating. However, thanks to the forced ventilation of the condenser placed
4 near to the compressor, a greater superheating of the refrigerant along the
5 suction line does not involve high compressor discharge temperatures to the
6 benefit of its reliability. The employed refrigerator is equipped with an adaptive
7 defrost system, realised using electric resistors arranged in the vicinity of the
8 evaporator. An electronic control system activates a defrost procedure that
9 consists in interrupting the power supply of the compressor and in turning on
10 the electric resistances. In so doing, the frost melts while the air temperature in
11 the freezer rises. During the defrost procedure, the frost melted is ducted to the
12 exterior of the cabinet and collected in a water tray in which are embedded a few
13 coils of the condenser. At the end of defrosting, the compressor is turned on, and
14 the cooling process restarts under a new and severe unsteady state condition:
15 this time the refrigeration duty has to overcome an additional thermal load
16 connected to the raising of the temperature in the freezer occurred during the
17 defrosting. However, the frost melted collected in the water tray facilitates the
18 cooling of the refrigerant at the condenser, reducing in part the increase in
19 energy consumption.
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22 *Fig. 2 Sketch of the refrigeration circuit*
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24 **2.2. Sensors and instrumentations**

25 A set of sensors and instrumentation has resulted in the characterization of
26 the refrigerator before and after the drop-in. The use of the PT100 at entry and
27 exit of each component of the system has allowed for monitoring the
28 temperature of the refrigerant in the key points of the plant. The thermo-
29 resistances were located outside the pipe, with a layer of heat transfer

1 compound (aluminium oxide plus silicon) placed between the sensor and the
 2 pipe to provide proper thermal contact. The entire pipe was covered with 25 mm
 3 thick flexible insulation. The system of temperature measurement was checked
 4 against a sensor positioned in a pocket in a similarly insulated pipe. For various
 5 test conditions, the difference between the two measurements always resulted in
 6 less than 0.3 °C. To monitor the air temperature within the compartments, in
 7 each of them a thermo-resistance was placed in proximity of the thermometer,
 8 which the manufacturer placed to control the working of the refrigerator. The
 9 temperature measurement obtained by this configuration was compared with
 10 that achieved by placing a PT100 at different points. For various test conditions,
 11 the difference between the two measurements was less than 1.0 °C.

12 By neglecting the pressure drops through the heat exchangers, the
 13 evaporating pressure and the condensing pressure were measured using a
 14 couple of piezoelectric sensors, each of them placed respectively at the suction
 15 and the discharge of the compressor. An energy metre allowed to measure both
 16 the electric energy and the electric power absorbed by the refrigerator during
 17 the tests. A thermo-hygrometer allowed for monitoring the temperature and
 18 relative humidity of the air surrounding the cabinet. To measure the different
 19 refrigerant charges an electronic balance able to appreciate variations in mass of
 20 0.1 g was used. Each sensor was connected to a 32-bit A/D acquisition system
 21 attached to a personal computer that allows a sample rate up to 10 kHz. A
 22 virtual instrument called FrigoCheck and realised in LabView, allowed for
 23 monitoring and recording each measurement during the tests. Additionally, by
 24 resorting to pressure and temperature measurements made in steady state
 25 conditions and by using the RefProp 9.1 software [38], for both refrigerants has
 26 been possible to calculate the enthalpy value. For different operating conditions
 27 and both examined fluids, in agreement with Moffat [39], it was estimated for the
 28 enthalpy an accuracy contained in the range: 1.10-1.95%. Tab. 3 contains further
 29 information on the sensors and the instruments used.

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Transducers	Range	Uncertainty
PT100 4 wires	-100 ÷ 500 °C	± 0.15°C
Humidity sensor	-100 ÷ 70 °C / 0 ÷ 100%	± 0.15°C / ± 1.0%
Piezoelectric absolute pressure gauge	1 ÷ 10 bar; 1 ÷ 30 bar	± 0.2% ± 0.5% F.S
Energy meter	0 ÷ 1 MWh	± 1 %
Balance	0 ÷ 100 kg	± 0.1 g

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Tab. 3 Characteristics of the sensors and instrumentations employed.

2.3. Experimental procedure

All tests have been developed following UNI-ISO 15502: 2005 concerning conditions for subtropical regions. The refrigerator is housed in a climate chamber capable of maintaining the air temperature at $+ 25 \text{ }^\circ\text{C} \pm 0.5 \text{ }^\circ\text{C}$ and the relative humidity in the range 45-75%. The freezer set-point has been set to $-18 \text{ }^\circ\text{C}$. The refrigerator thermostat has been adjusted so as to maintain the temperature at $+ 5 \text{ }^\circ\text{C}$. In agreement with what has been shown by Bansal [40] and Hermes [41] it was decided not to take the test pack within of refrigeration compartments, leaving, therefore, the typical inertial phenomena of the thermal load due to the foods and not to the thermodynamic characteristics of the refrigerants. The investigation was divided into two phases:

1. Operating system characterization with R134A as built, to identify the conditions of reference to compare with those obtained following the drop-in;
2. Characterization of the system operating with HFO1234YF.

For each step, two kinds of tests were carried out:

- Pull down: the plant started under the condition of thermal and hygrometric equilibrium between the air surrounding the cabinet and the air inner to the compartments, and all quantities reported in 2.2 were recorded. When the first shutdown of the compressor occurred, the elapsed time to achieve a temperature of -18°C in the freezer compartment was stored.
- 1-day consumption: starting under steady state condition, for which the compressor times to cycle ON and OFF kept happening with a maximum deviation of 5% each other, all quantities reported in 2.2 were recorded for 24 consecutive hours. Following the instructions reported in the UNI-ISO 15502:2005, if at least one defrost procedure happened, the test was considered valid. Also, it was evaluated the average duty cycle using the following equation:

$$\delta = AVERAGE \left(\frac{t_{ON}}{t_{ON}+t_{OFF}} \right) \quad (1)$$

where t_{ON} and t_{OFF} are respectively the time when the compressor has been working (ON phase) and when the compressor has been kept off (OFF phase).

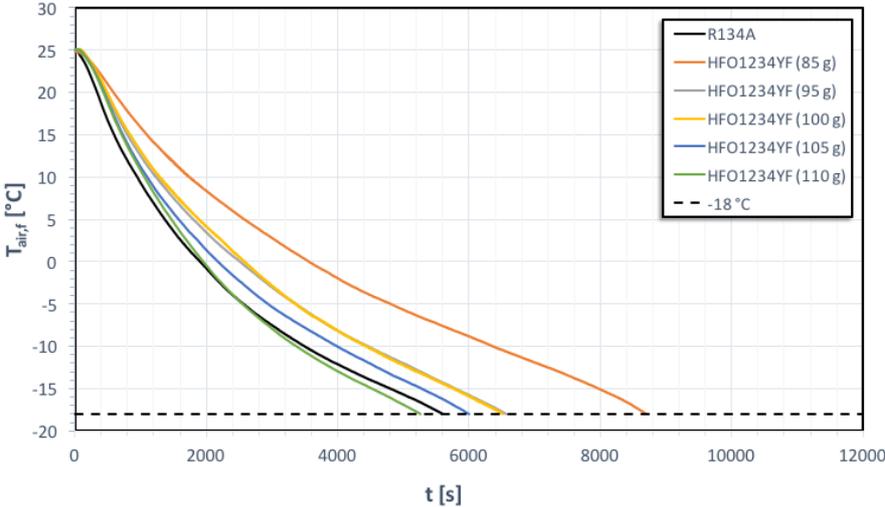
Not being known a priori the optimal charge of HFO1234YF it was imperative a survey to its detection. To this end, starting with a charge of HFO1234YF equal to 85 g, it has been realised a series of pull-down tests obtained adding 5 g of the refrigerant at a time.

3. Results and discussions

3.1. Pull down tests

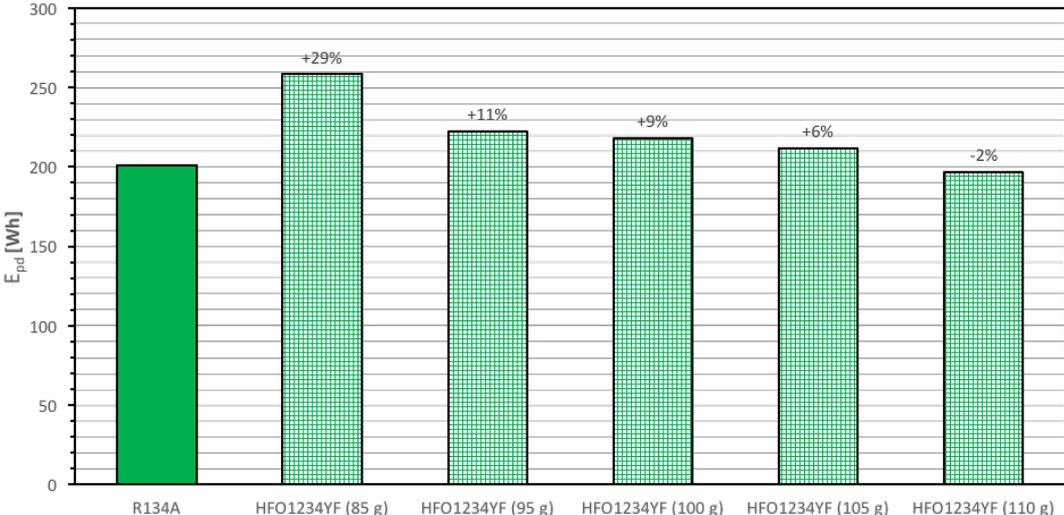
Fig. 3 shows the profiles of air temperature inside the freezer ($T_{\text{air},f}$) recorded during the pull-down tests for R134A and different charges of HFO1234YF. By

1 using R134A, the refrigerator has employed 5'650 s to reach a $T_{air,f}$ equal to -18
 2 °C. As a consequence of the drop-in with the HFO1234YF, the plant has changed
 3 the pull-down time. In particular, for a mass equal to 105g a delay of 408 s (+7.0
 4 %) has been recorded, while adopting 110g the pull-down time has been
 5 reduced by 410 s (- 7.3 %)
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 8 *Fig. 3 Temperature profiles of the air inside the freezer compartment*
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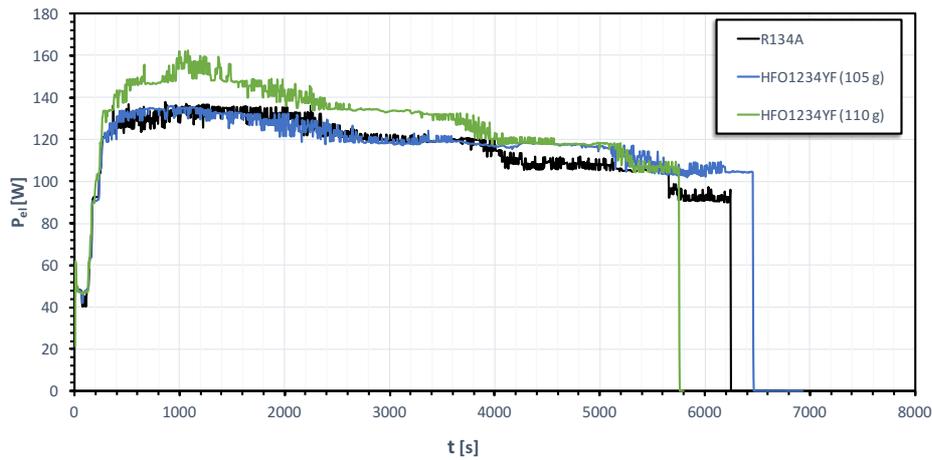
10 The increase of HFO1234YF mass has led to a variation of electrical energy
 11 consumptions due to the pull-down test (E_{pd}). It has been noted (Fig.3 and Fig.4)
 12 by increasing the charge of HFO1234ZE the reduction of the pull-down time has
 13 not been accompanied by a considerable reduction of the electrical energy
 14 consumption compared to R134A. In particular, an HFO1234YF mass equal to
 15 110g has led to a 2% reduction of E_{pd} , which is nearest to the accuracy of the
 16 energy meter used (Tab. 3).



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 18 *Fig. 4 Electric energy consumption during the pull-down tests*
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When the overall mass of HFO1234YF is equal to 110g, the compressor has absorbed a higher electric power (P_{el}) than that absorbed adopting a mass equal to 105g (Fig.5). At the same time, the greater mass of HFO1234YF has led to a maximum peak of condensation pressure: 16.1 bar against 12.5 bar. The highest pressure peak value suggests that a further add of refrigerant mass might have been exceeding. Consequently, because the refrigerant charge equal to 110g has resulted both in an energy and in a pull-down time saving, it has been taken as the optimal mass.

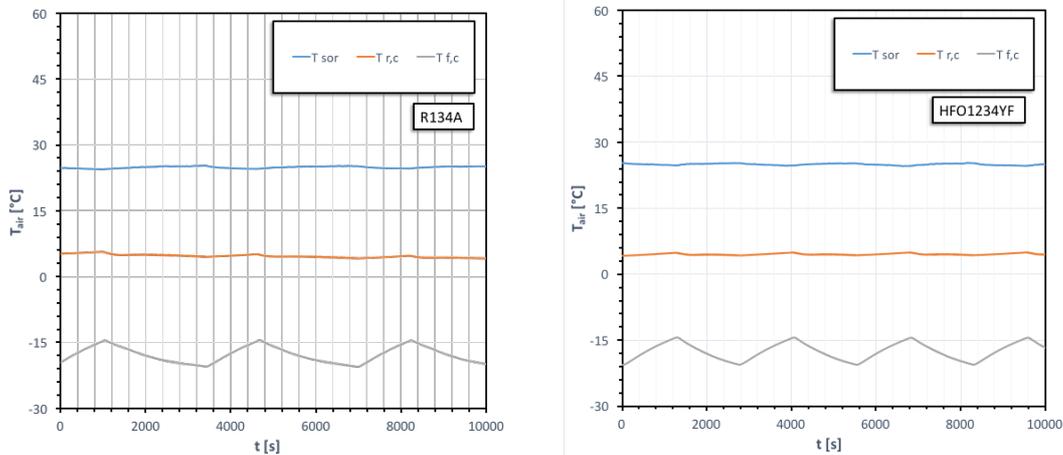


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Fig. 5 Electric power absorbed during the pull-down tests

3.2. 1-day tests

Identified the optimal charge for the HFO1234YF, it proceeded with the second phase of the experimentation. In Fig.6 for both refrigerants are reported a test sample long 10'000 s. The profiles there reported show the change of the air temperature inside the freezer ($T_{f,c}$), inside the refrigerator ($T_{r,c}$), and surrounding the cabinet (T_{sor}). It is possible to note the respect of the test conditions given in 2.3, together with the relative humidity variation contained in the range 45-68% (following UNI-ISO 15502: 2005).



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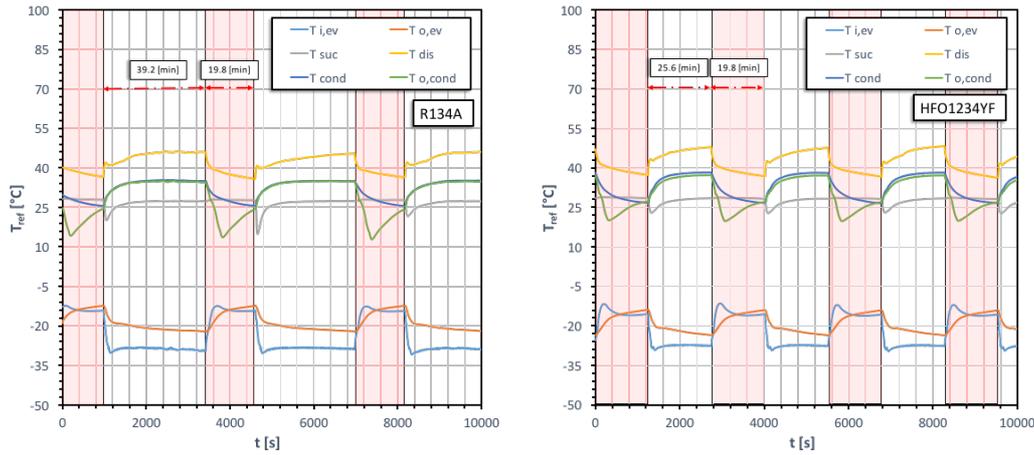
Fig. 6 Air temperature profiles during a sample of the 1-day test.

1 In particular, due to the act of the thermostat that regulates the working of the
2 refrigerator, the $T_{f,c}$ has changed between $-21\text{ }^{\circ}\text{C}$ and $-15\text{ }^{\circ}\text{C}$, with a mean value
3 equal to $-18\text{ }^{\circ}\text{C}$, while the $T_{r,c}$ has undergone smallest variations around the value
4 $+5\text{ }^{\circ}\text{C}$. Such behaviour is justified by the greater thermal power dispersed
5 through the walls of the freezer compartment than that dispersed through the
6 walls of the refrigerator compartment. In fact, even if the $U \cdot S_{cab}$ of the freezer
7 compartment is less than that of the refrigerator compartment (Tab. 2), the
8 freezer has been affected by higher thermal dispersion because of the higher
9 difference between T_{sor} and $T_{f,c}$.

10 For the same test sample, Fig. 7 shows the refrigerant temperature profiles
11 obtained at the key points of the plant, in addition to the representation of ON
12 and OFF cycles of the compressor. By considering the Eq. 1, as a first result of the
13 analysis, one can note that HFO1234YF has allowed for a reducing of the duty
14 cycle: 50.6% against 66.0%. Accordingly, since the loading conditions for both
15 refrigerants have been the same, it can be supposed that HFO1234YF developed
16 a greater cooling capacity.

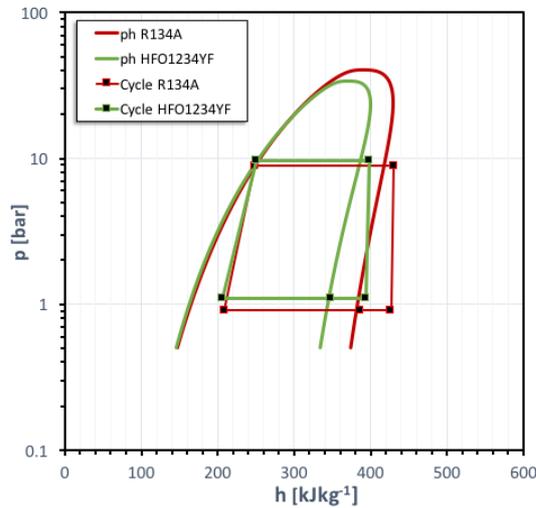
17 Looking at the ON phases and focusing on steady-state condition
18 (approximately after 10 minutes), in the low-pressure zone of the plant one can
19 observe slight deviations for the temperatures recorded for both refrigerants; in
20 any case, the differences are contained within a narrow range equal to $1.5\text{ }^{\circ}\text{C}$.
21 Contrary, HFO1234YF has caused an increase in the temperature levels in the
22 high-pressure zone of the plant. In particular, the condensation temperature of
23 HFO1234YF has been 3°C greater than that of R134A. Regarding the working
24 pressures, the drop-in has led to a slight increase in evaporation pressure (1.11
25 bar against 0.91 bar) and higher condensation pressure (9.73 bar against 8.88
26 bar). However, when HFO1234YF is used, a compression ratio (p_{dis}/p_{suc}) equal to
27 8.8 occurred, which was 12% less than that of R134A. A lower compression ratio
28 suggests that compressor operating with HFO1234YF was subjected to a higher
29 volumetric efficiency. Looking at the thermodynamic properties of both
30 refrigerants [38] and considering the corresponding thermodynamic state at the
31 suction of the compressor, it is worthy to evidence the higher density reached by
32 HFO1234YF: 5.2 kg m^{-3} against 3.8 kg m^{-3} . The better volumetric efficiency and
33 the higher density at the suction of compressor suggest HFO1234YF has led to a
34 mass flow rate greater than that obtained with R134A. To better understand the
35 consequence of the mass flow rate increasing, one has to wonder what happened
36 at evaporator regarding enthalpy. Looking at Fig. 8, as a result of the drop-in,
37 one can note a significant reduction of the enthalpy variation at the evaporator ($-$
38 20.1%), but, at the same time, the superheat degree has experimented a
39 reduction (2.6°C) as well. The decrease of the duty cycle, the increasing of the
40 mass flow rate, and the superheat degree demonstrate that drop-in with
41 HFO1234YF has allowed for augmenting the cooling capacity of the fridge.

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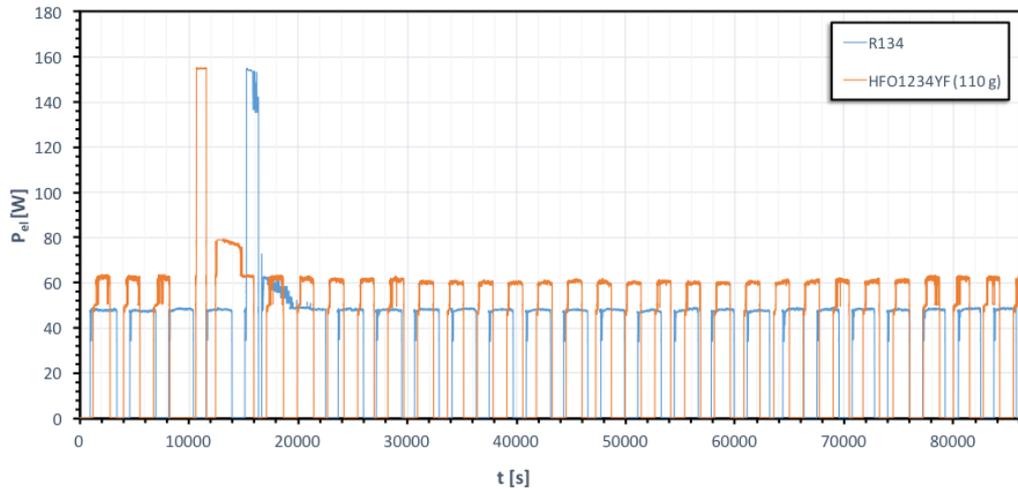
Fig. 7 Refrigerant temperature profiles at different points of the plant during a sample of a 1-day test; the red bands represent the OFF phase.



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Fig. 8 Representation in the p-h plan of the thermodynamic cycle during the steady state conditions

9 By observing the compression phase plotted in Fig. 8, it is evident the
10 influence of the air ventilation employed for the condenser (as described in 3.1).
11 For both refrigerants, the difference of the enthalpy between the inlet and the
12 outlet of the compressor has been slight. In particular, HFO1234YF has led to a
13 greater specific compression work ($5.01 \text{ kJ kg}^{-1}\text{K}^{-1}$ against $3.35 \text{ kJ kg}^{-1}\text{K}^{-1}$), which,
14 together a higher discharge temperature, suggests a worst isentropic efficiency
15 of the compressor. This phenomenon and the higher mass flow rate justify the
16 higher electric power absorbed (Fig.9) by the compressor after the drop-in: 60.2 W
17 against 50.8 W . In a similar way, one can validate what previous has been
18 reported in Fig. 5 as well.

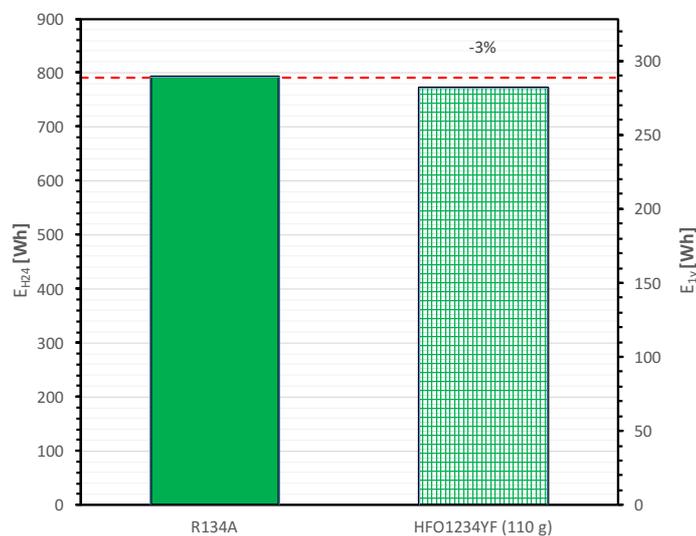


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2 *Fig. 9 Electric power absorbed during the 1-day tests and highlighting of*
3 *defrosting phase as required by the test conditions given in 2.3.*
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5 However, the higher electric power absorbed after the drop-in has not led to
6 an increase of the energy consumptions. In fact, a better energy performance due
7 to HFO1234YF can be seen in Fig. 10, where are reported the electric energy
8 consumptions recorded over a 24-hours test and the projections of annual
9 consumptions, calculated as follows:

10
$$E_{1y} = E_{H24} \times 365 \text{ days} \quad (2)$$

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12
13 *Fig. 10 Daily and yearly energy consumptions for both refrigerants.*
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15 After 24 hours of working with HFO1234YF, the plant has recorded an energy
16 saving equal to 3%. Although this result is connected to the particular conditions
17 adopted in this experimentation, it is likely that the energy saving recorded can
18 also be expected in the presence of openings and closings of the door as happens
19 in reality, because the dynamic behaviour of the plant has been the same for both

1 refrigerants. It is worthy to note that such energy saving has to be attributed not
2 only to the fluid but also to the optimization of the charge made in the present
3 study. In fact, it is right to mention that under different circumstances, other
4 researchers [18,28,29] showed that HFO1234YF can lead to an increase in
5 energy consumptions when compared to R134a. On the contrary, as suggested
6 by Bansal [40], HFO1234YF can offer up to 5% energy saving with simple cycle
7 modifications. However, even if the energy saving, achievable as a result of a
8 drop-in with HFO1234YF, was negligible, it should be noted that such a
9 refrigerant allowed for preserving the operating conditions of the plant analysed,
10 except the limitation due to a lower saturation pressure. Considered, therefore,
11 the reduced GWP value of HFO1234YF, it can be said that such refrigerant may
12 be one of the potential candidates to replace R134A in domestic refrigerators,
13 both for plants already in operation and for new devices. Furthermore, the
14 adoption of HFO1234YF would be at zero cost for the manufacturers of the
15 household refrigerators. In fact, such as it has been shown here, it is not
16 necessary to make any changes to the cooling circuit of a plant designed to
17 operate with R134A, but it highlights only the need to achieve an optimization
18 for the HFO1234YF charge.

19

20 **4. Conclusions**

21 In this paper an experimental comparison between R134A and HFO1234YF
22 has been presented, when they are used as refrigerants for a domestic
23 refrigerator. In particular, the analysis was carried out by operating the drop-in
24 of R134A with HFO1234YF in a commercial plant of the type frost free and
25 provided with a freezer and a refrigerator compartment. The analysis, conducted
26 under temperature and humidity controlled, has been realised using two kinds of
27 tests: pull down for the identification of the optimal charge of HFO1234YF and 1-
28 day for the detection of the electric energy consumption. Regarding the test
29 conditions and to the plant analysed, it can be concluded that:

- 30 ▪ The drop-in of R134a with HFO1234YF maintains the functionality of the
31 plant regarding the temperature reached in the refrigerating compartments.
- 32 ▪ The charge of HFO1234YF which preserves the behaviour of the plant
33 regarding the temperature pull-down time has resulted greater than 10% of
34 that of R134a.
- 35 ▪ HFO1234YF has allowed for reducing of a 7.3 % the pull-down time and of a
36 23% the duty cycle.
- 37 ▪ HFO1234YF has led to a higher condensation pressure but to a higher mass
38 flow rate thanks to a better volumetric efficiency and a greater density at the
39 suction of the compressor.
- 40 ▪ HFO1234YF has allowed for an increasing of the cooling capacity.
- 41 ▪ A worst isentropic efficiency of the compressor has been observed when
42 HFO1234YF is used. Although, after 24 hours of working a 3% energy saving
43 has been obtained.

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- HF01234YF can be used in plants already in operation (drop-in) and as a refrigerant for new devices.

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