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Abstract: Environmental contamination by pharmaceuticals is an emerging issue. Even if pharmaceuticals are present at very low concentrations in the aqueous environment, they make implications for human health, giving rise to phenomena of bacterial resistance. Among antibiotics, spiramycin is today used to treat a wide variety of infections. Heterogeneous photocatalytic processes in presence of UV light are successful to obtain complete mineralization of various pharmaceutical pollutants but no one has studied the photocatalytic removal of spiramycin under visible light irradiation. In this work N-doped TiO<sub>2</sub> photocatalysts active under visible light was used to evaluate the photodegradation of this antibiotic. Photocatalytic tests were carried out in a slurry photoreactor irradiated both with UV lamps and blue LEDs with spectrum emission in the visible region. Reaction products in gas-phase were monitored by continuous analyzers, measuring CO and CO<sub>2</sub> gaseous concentrations at the photo-reactor outlet. The only product detected during irradiation was CO<sub>2</sub> confirming that the photocatalytic process has been proven effective in the mineralization process of spiramycin, reaching very high values of TOC removal.

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Kind Editor,

We are submitting the attached manuscript for publication in “**Chemical Engineering Journal special edition on Advances in Photocatalysis**”.

In the following I report the invitation letter from the guest Editor.

Best regards

Diana Sannino (e-mail: [dsannino@unisa.it](mailto:dsannino@unisa.it))

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*Sent: Tuesday, September 17, 2013*

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*Subject: Invitation to Submit an article to the Chemical Engineering Journal- Special issue on 'Photocatalysis for contaminants and microorganisms of emerging concern'*

*On behalf of the organising committee of JEP-2013 and the Editor of Chemical Engineering Journal, Professor D. Dionysiou, we would like to inform you that the Chemical Engineering Journal will be publishing a special issue in the area of 'Photocatalysis for contaminants and microorganisms of emerging concern'. As the guest editors of the special issue, we have noticed that you have previously published research related to environmental nanotechnology. Therefore, we would like to invite you to contribute a review article or a full research paper for peer-review and possible publication.*

*The subjects of the special issue include but not limited to environmental photocatalytic nanotechnology, depollution technologies using nanomaterials, AOPs/AON (Advanced oxidation technologies and nanotechnologies) on contaminants of emerging concern (pharmaceuticals, pesticides, cyanotoxins, etc), environmental sustainable nanotechnologies, and risk assessment and policy analysis of environmental technologies related to pollutants of emerging concern.*

*Sincerely Yours, Guest Editors*



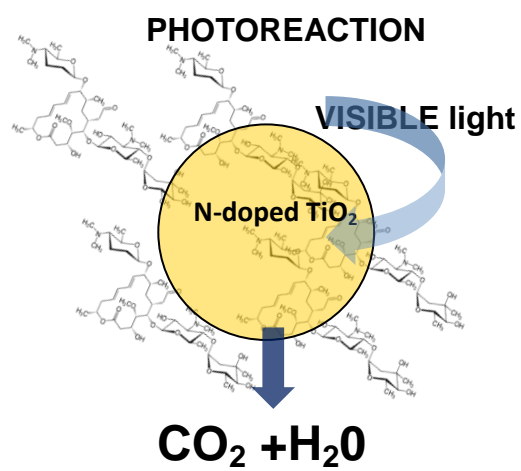
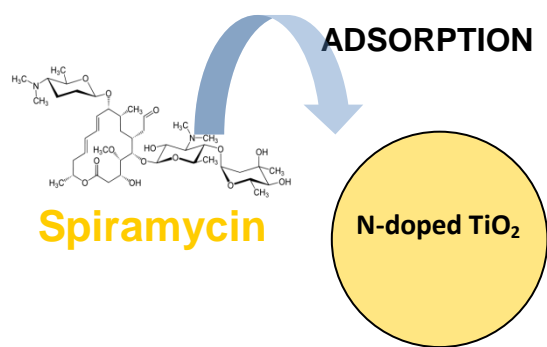
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## \*Highlights (for review)

- N-doped TiO<sub>2</sub> photocatalyst active under visible light irradiation.
- Photocatalytic mineralization of spiramycin under visible light irradiation.
- The only reaction product detected in gas-phase was CO<sub>2</sub>.
- Kinetic evaluations in different operating conditions.
- High photocatalytic mineralization of spiramycin of a real pharmaceutical wastewater

1           **Photocatalytic removal of spiramycin from wastewater**  
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3           **under visible light with N-doped TiO<sub>2</sub> photocatalysts**  
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15 **Abstract**

16 Environmental contamination by pharmaceuticals is an emerging issue. Even if  
17 pharmaceuticals are present at very low concentrations in the aqueous environment,  
18 they make implications for human health, giving rise to phenomena of bacterial  
19 resistance. Among antibiotics, spiramycin is today used to treat a wide variety of  
20 infections. Heterogeneous photocatalytic processes in presence of UV light are  
21 successful to obtain complete mineralization of various pharmaceutical pollutants but  
22 no one has studied the photocatalytic removal of spiramycin under visible light  
23 irradiation. In this work N-doped TiO<sub>2</sub> photocatalysts active under visible light was  
24 used to evaluate the photodegradation of this antibiotic. Photocatalytic tests were  
25 carried out in a slurry photoreactor irradiated both with UV lamps and blue LEDs  
26 with spectrum emission in the visible region. Reaction products in gas-phase were  
27 monitored by continuous analyzers, measuring CO and CO<sub>2</sub> gaseous concentrations  
28 at the photo-reactor outlet. The only product detected during irradiation was CO<sub>2</sub>  
29 confirming that the photocatalytic process has been proven effective in the  
30 mineralization process of spiramycin, reaching very high values of TOC removal.

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32 **Keywords:** Photocatalysis; spiramycin; N-doped TiO<sub>2</sub>; visible light; UV light;  
33 Langmuir-Hinshelwood kinetics; real pharmaceutical wastewater.

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## 35 Introduction

36 Pharmaceutical active compounds (PACs) have attracted much attention in recent  
37 years due to their adverse effects towards natural organisms and potential effects on  
38 human beings. The traditional plants for treatment of wastewater are able to remove  
39 microbes and organic matter, while the pharmaceuticals compounds are not oxidized.  
40 As a consequence, when this effluent is released from the treatment plants into an  
41 aquatic body, drug-tainted waters are introduced directly into the aquatic habitat.  
42 Thus PACs are progressively accumulated into the environment. In fact, several  
43 studies carried out in the past few years, have demonstrated the presence of PACs in  
44 groundwater, surface water and even in drinking water [1-5]. These drug-tainted  
45 waters must be treated for human consumption or for different human activities [6,  
46 7].

47 Advanced oxidation processes (AOPs), such as ozonation, Fenton, photo-Fenton  
48 oxidation, and heterogeneous photocatalysis [8-16] have shown great efficiency in  
49 recent years as possible future complementary methods to conventional wastewater  
50 treatments [17-19]. Among these AOPs, TiO<sub>2</sub> photocatalysis is under developing as  
51 an affordable, effective, environmentally friendly and sustainable technology for  
52 various chemical transformations [20-28]. Several studies have demonstrated that  
53 ultraviolet (UV) and visible light is able to decompose pharmaceuticals by direct  
54 photolysis or indirect photolysis through an AOP. Indeed, Amoxicillin [29],  
55 nitroimidazoles [30], oxytetracycline [31], and sulfamethoxazole [32] are degraded  
56 by UV or visible light treatments.

57 Among antibiotics, spiramycin (SP) (Figure 1) is a macrolide antibiotic used to treat  
58 infections of the oropharynx, respiratory system, genito-urinary tract, as well as

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59 cryptosporidiosis and toxoplasmosis [33]. Similarly to the other antibiotics AOPs can  
60 be applied to remove SP from water.  
61 SP degradation has been reported under UV light irradiation in presence of TiO<sub>2</sub>  
62 [34], but no one has studied photocatalytic removal of SP under visible light  
63 irradiation.  
64 However, to reach this goal, it is necessary to modify titanium dioxide in order to  
65 make it able to exploit visible light. This feature can be realized by doping TiO<sub>2</sub>  
66 crystal lattice with various elements. Among such modified materials, N-doped  
67 TiO<sub>2</sub>, under visible light, exhibits stable characteristics and performance in  
68 wastewater treatment applications [35, 36]. The use of visible light would represent,  
69 then, a more economical alternative. For this reason the objective of this study is to  
70 explore the possibility of using blue LEDs as source of visible light for the  
71 photocatalytic removal of SP. The effect of various parameters, such as SP  
72 concentration and type of light sources was investigated.

## 73 74 **1. Materials and methods**

### 75 *2.1 Materials*

76 N-doped TiO<sub>2</sub> (Nt) photocatalyst was prepared by the hydrolysis reaction between  
77 the titanium tetraisopropoxide and an aqueous solution containing ammonia. More in  
78 detail, a volume of 100ml ammonia aqueous solution at 30wt %, supplied by Carlo  
79 Erba, was quickly added to 25ml of 97wt% titanium tetraisopropoxide (TTIP by  
80 Sigma Aldrich) at 0°C during a vigorous stirring of the solution in which a white  
81 precipitate was progressively formed. The precipitate was then carefully washed with  
82 bidistilled water and centrifuged to be separated. After the separation of settle solids,  
83 the obtained powders were dried and calcined at 450°C for 30 minutes, yielding N-

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84 doped TiO<sub>2</sub> in anatase phase. The band–gap energy of titanium dioxide was then  
85 moved in the visible range from 3.3eV to 2.5eV [35]. The final N/Ti molar ratio was  
86 equal to 18.6 and corresponds to an optimized catalyst formulation, as found in  
87 previous works devoted to the optimization of doping process and to the evaluation  
88 of photocatalytic activity towards organic dyes [37].

89 A SP source, commercial antibiotic pills, was provided by Mylan generics.

90

## 91 *2.2. Photocatalytic tests*

92 Aqueous solutions containing SP were prepared using weighted fractions of pills  
93 dissolved in bidistilled water, to get a more realistic drug-tainted wastewater.

94 The experiments were realized using a pyrex cylindrical photoreactor (ID= 2.5 cm)  
95 equipped with an air distributor device ( $Q_{\text{air}}=250\text{cm}^3/\text{min}$  (STP)), magnetic stirrer to  
96 maintain the photocatalyst suspended in the aqueous solution and temperature  
97 controller. The photoreactor was irradiated with a strip composed by 25 blue LEDs  
98 (BL strip) (provided by NEW ORALIGHT; nominal power: 5W) with wavelength  
99 emission in the range 400–550 nm [35, 37] or with four UV lamps (provided by  
100 Philips; nominal power: 32 W) with wavelength emission at 365nm. The light  
101 sources were positioned around the external surface of the photoreactor (Figure 2).

102 In a typical photocatalytic test, 3 g/L of photocatalyst was suspended in 100mL  
103 solution. The system was left in dark condition for 2 hours to reach SP adsorption  
104 equilibrium on catalyst surface, and then photocatalytic reaction was initiated under  
105 visible or UV light up to 7 h. Samples were taken during the tests and centrifuged for  
106 removing powders from the SP solution. The analysis of gas phase coming from the  
107 photoreactor was performed by means of a continuous CO, CO<sub>2</sub>, non-dispersive  
108 infrared analyser (ABB Advance Optima).

109 The photocatalytic activity was tested in terms of the reduction of total organic  
110 carbon (TOC) that is a parameter able to analyze SP mineralization. TOC of solution  
111 has been measured from CO<sub>2</sub> obtained by catalytic combustion at T=680°C. CO<sub>2</sub>  
112 produced in gas-phase was monitored by continuous analyzers, measuring CO, CO<sub>2</sub>  
113 (Uras 14, ABB) and O<sub>2</sub> (Magnos 106, ABB) gaseous concentrations [8].

114 The natural pH of solution was equal to about 6 and the temperature was controlled  
115 being in the range 20-30°C. Finally, the performances of Nt photocatalyst in  
116 presence of visible light were tested in the photocatalytic treatment of a real  
117 pharmaceutical wastewater containing SP with an initial TOC content of about 20  
118 mg L<sup>-1</sup>.

119

### 120 **3. Results and Discussion**

#### 121 *3.1 Influence of photocatalyst and different light sources*

122 Preliminary experiments were carried out in order to verify that SP was degraded  
123 by heterogeneous photocatalytic process. In the absence of Nt, no significant  
124 decrease in TOC was observed during the 7h of illumination both with UV light and  
125 visible light irradiation (Figure 3). In particular, TOC removal was less than 10% in  
126 the case of visible light irradiation and 19% in the case of UV light irradiation. So,  
127 photolysis phenomena occur but in a limited extent.

128 The TOC profiles as function of irradiation time obtained in the presence and in the  
129 absence of Nt under the irradiation realized by UV lamps are reported in Figure 4. In  
130 dark conditions, a decrease of TOC was observed during the first hour of the test and  
131 it was unchanged in the second hour, indicating that the adsorption equilibrium of SP  
132 on catalyst surface was reached. After the dark period, the solution was irradiated

133 with UV light and the reaction started to occur. It can be seen that TOC value was  
134 lower when UV light was applied in the presence Nt photocatalyst. In fact, a final  
135 TOC removal reached a value of about 48%, so remarkably improved in comparison  
136 to photolysis alone.

137 The analysis of gases coming from the photoreactor showed the presence of only  
138 CO<sub>2</sub> during the UV light irradiation, confirming the occurring of the mineralization  
139 of SP (Figure 5). It is important to underline that no formation of CO<sub>2</sub> was detected  
140 in absence of light irradiation. This last experimental result shows that the TOC  
141 reduction obtained in dark conditions was due to only adsorption of SP on Nt  
142 surface.

143 Through a comparison between the amount of carbon consumed during the  
144 photocatalytic reaction (as assessed by TOC analysis) and the amount of carbon  
145 released as CO<sub>2</sub>, the total carbon mass balance was closed to about 95±5%,  
146 evidencing that SP is selectively converted to CO<sub>2</sub>. It is possible to affirm that total  
147 mineralization of SP was obtained in presence of photocatalyst.

148 It was also performed visible light driven photocatalytic removal of SP over the Nt  
149 using the light emitted by BL and results are presented in Figure 6. It is observed that  
150 SP photolysis shows a progressive removal of TOC up to a value lower than 10%  
151 after 7 h of irradiation. In contrast, the presence of Nt showed higher removal rate  
152 with a final TOC removal of 45 % after 6 h of irradiation. This enhanced  
153 photocatalytic ability in presence of visible light is ascribed to nitrogen insertion in  
154 the crystalline structure of titania.

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156

157 *3.1 Effect of Spiramycin concentration*

158 The effect of the SP concentration has been studied with an initial TOC ranging  
159 between 40 and 170 mgL<sup>-1</sup>. The mineralization in terms of TOC removal achieved  
160 after 4 hours under the visible light for 40, 60, and 170 mgL<sup>-1</sup> of initial TOC, were  
161 74, 68, and 40%, respectively (Figure 7).

162 *3.2 Kinetic modelling*

163 *3.2.1 Adsorption in dark conditions*

164 For the evaluation of SP adsorption on the active surface [38], the following equation  
165 was used:

$$166 \quad TOC^* = \frac{b \cdot TOC_d}{1 + b \cdot TOC_d} \quad \text{Eq. 1}$$

167 Where:

168 TOC\*: amount of SP adsorbed on catalyst in dark conditions [g /g]

169 TOC<sub>m</sub>: maximum absorbable value of TOC\*

170 TOC<sub>d</sub>: concentration of SP in solution after dark adsorption [mg L<sup>-1</sup>]

171 b: adsorption equilibrium constant [L mg<sup>-1</sup>]

172 Eq.1 can be rearranged to give:

$$173 \quad \frac{TOC_d}{TOC^*} = \frac{1}{b \cdot TOC_m} + \frac{1}{TOC_m} \cdot TOC_d \quad \text{Eq. 2}$$

174 Accordingly, a plot of TOC<sub>d</sub>/TOC\* as a function of TOC<sub>d</sub> produces a straight line  
175 with: slope=1/TOC<sub>m</sub> and intercept=1/b\*TOC<sub>m</sub> (Figure 8).

176 The value of b was calculated from Eq. 2 utilizing the data reported in Figure 8 and  
177 it was equal to 0.0089 [L mg<sup>-1</sup>].

178 3.2.2 Evaluation of rate constant

179 The mathematical model has been realized considering that in the batch reactor under  
180 blue LEDs irradiation, occur mainly the total oxidation of SP to CO<sub>2</sub>.

181 Mass balance on SP concentration (expressed as TOC) can be written as:

182 
$$V \cdot \frac{dTOC(t)}{dt} = r(TOC, I) \cdot W_{Nt}$$
 Eq. 3

183 Where:

184 TOC(t) : TOC at given reaction time, [g L<sup>-1</sup>]

185 -r: reaction rate, [g L<sup>-1</sup> h<sup>-1</sup>]

186 W<sub>Nt</sub>: amount of catalyst effectively irradiated [35, 37], [g]

187 The initial conditions are:

188 t=0 TOC=TOC<sub>0</sub>

189 The kinetic expressions is well described with the classic Langmuir- Hinshelwood  
190 (L-H) mechanism [39] in terms of mineralization of SP as in the following:

191 
$$-r = K \cdot \frac{b \cdot TOC}{1 + b \cdot TOC} \cdot \frac{I \cdot \alpha}{1 + I \cdot \alpha}$$
 Eq. 4

192 Where:

193 K=kinetic constant [mg g<sup>-1</sup> h<sup>-1</sup>]

194 α= light absorption coefficient [cm<sup>2</sup> mW<sup>-1</sup>]

195 I= light intensity reaching the photocatalyst surface [mW cm<sup>-2</sup>].

196 Eq. 4 is similar to the Langmuir-Hinshelwood rate law used in other studies  
197 regarding the mathematical modelling of methylene blue degradation [37].



198 This equation takes into account also the influence of light intensity. In fact, only a  
199 fraction of nominal radiation reaching the photocatalyst particles is absorbed by  
200 itself. This effect was considered utilizing the parameter  $\alpha$ . This parameter depends  
201 only on the reactor configuration and light sources and not on the liquid medium; its  
202 value is equal to  $0.000925 \text{ [cm}^2 \text{ mW}^{-1}\text{]}$  and it is the same used in a previous work  
203 [37]. Moreover, it is important to consider that the light penetration inside the reactor  
204 core depends on type of pollutant (in this case SP) and on the catalyst concentration  
205 [37]. This suggests that only a part of the light intensity entering in the reactor, will  
206 be reach the photocatalyst particles. To consider this screening effect, a first order  
207 correlation (similar to Lambert-Beer law) for the effective light energy received by  
208 the Nt particles [37] was used:

$$209 \quad I = I_0 \cdot e^{-[Nt]k_I} \quad \text{Eq.5}$$

210 Where:

211  $k_I$ = specific extinction coefficient per unit catalyst mass [ $\text{L mg}^{-1}$ ]

212  $I$ = light intensity reaching the photocatalyst surface [ $\text{mW cm}^{-2}$ ].

213  $I_0$ = nominal light intensity=  $32 \text{ mW cm}^{-2}$

214  $[Nt]$ = catalyts dosage [ $\text{mg L}^{-1}$ ].

215 Eq. 4, coupled with Eq. 5, together with the initial condition, was solved with Euler  
216 iterative method to identify the constants K and  $k_I$  by fitting experimental data  
217 reported in Figure 9 as a function of irradiation time. The fitting procedure was  
218 realized by using the least squares approach obtaining the value of K:  $6.04 \text{ [mg g}^{-1} \text{ h}^{-1}$   
219  $]$ , and  $k_I$ :  $0.349 \text{ [L mg}^{-1}\text{]}$ . After obtaining the model parameters, the experimental  
220 data obtained with different initial TOC were fitted to analyse the ability of the

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221 model to predict the experimental data. The obtained results are shown in Figure 10.  
222 In this series of experiments, the incident light intensity ( $I_0$ ) and  $N_t$  dosage are kept  
223 constant. The calculated values in both cases are in good agreement with the  
224 experimental data. It is important to note that also for the higher  $TOC_0$  (170 ppm),  
225 this system is able to predict the mineralization trend with a single value of kinetic  
226 constant. This last result is in contrast with literature works about kinetic degradation  
227 of antibiotics in liquid phase that report different values for mineralization constant  
228 [32].

229

### 230 *3.3 Photocatalytic performance of $N_t$ under visible light on a real wastewater* 231 *coming from a pharmaceutical plant for production of spiramycin*

232

233 The treatment of real wastewater sample was effected because it could be more  
234 difficult its depollution due to the wide variety of the products in variable  
235 composition. The performances of  $N_t$  photocatalyst on real wastewater coming from  
236 a pharmaceutical plant for production of spiramycin was shown in Figure 11. In the  
237 case analyzed, the initial value of  $TOC_0$  was about  $20 \text{ mg L}^{-1}$ . In dark conditions the  
238 decrease of TOC was equal to 24%. After the dark period, visible light source was  
239 turn on and the mineralization process started determining a decrease of TOC. The  
240 value of TOC reached after 40 minutes of irradiation was about 3 ppm corresponding  
241 to almost 83 % of conversion.

## 242 **4. Conclusions**

243 The removal of spiramycin in N-doped  $TiO_2$  suspension was investigated for the first  
244 time under visible light. The results showed that the photocatalytic process seems to  
245 be very efficient in the mineralization of spiramycin. During irradiation time, the  
246 only product detected in gas phase was  $CO_2$  confirming that the photocatalytic

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247 process has been proven effective in the mineralization of spiramycin, reaching very  
248 high values of TOC removal. Kinetic evaluations evidenced that the mineralization  
249 process can be described with a single value of reaction constant, also at very high  
250 initial concentration of antibiotic.

251 The system is also able to mineralize the spiramycin and all the organic compounds  
252 present in a real pharmaceutical wastewater reaching high values of depollution in  
253 short times. Photocatalytic visible treatment of spiramycin containing streams with  
254 N-doped titania appeared a very promising method for wastewater treatment.

255

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Figure1

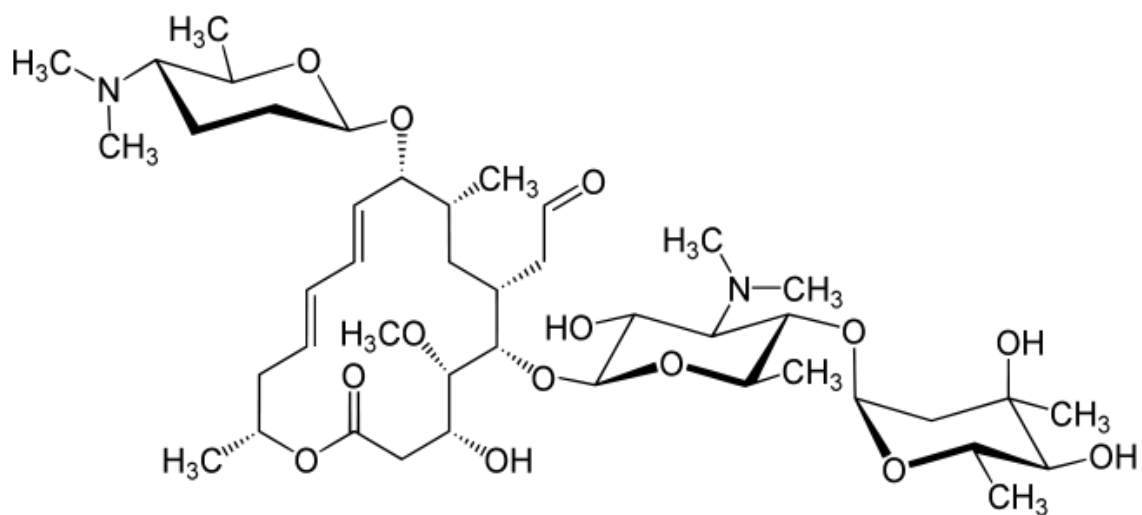
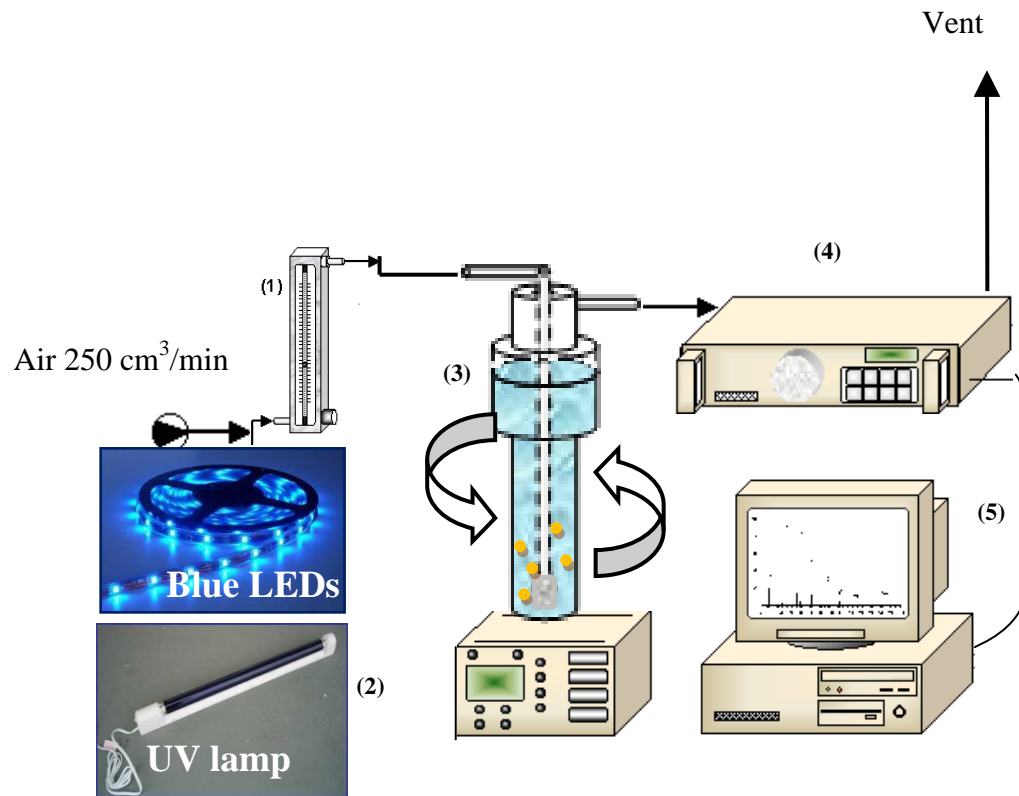


Figure 1 Chemical structure of SP



**Figure 2** Experimental set up apparatus (1) rotameter; (2) magnetic stirrer; (3) photoreactor; (4) CO,CO<sub>2</sub> analyzer, (5) personal computer for data acquisition.

Figure3

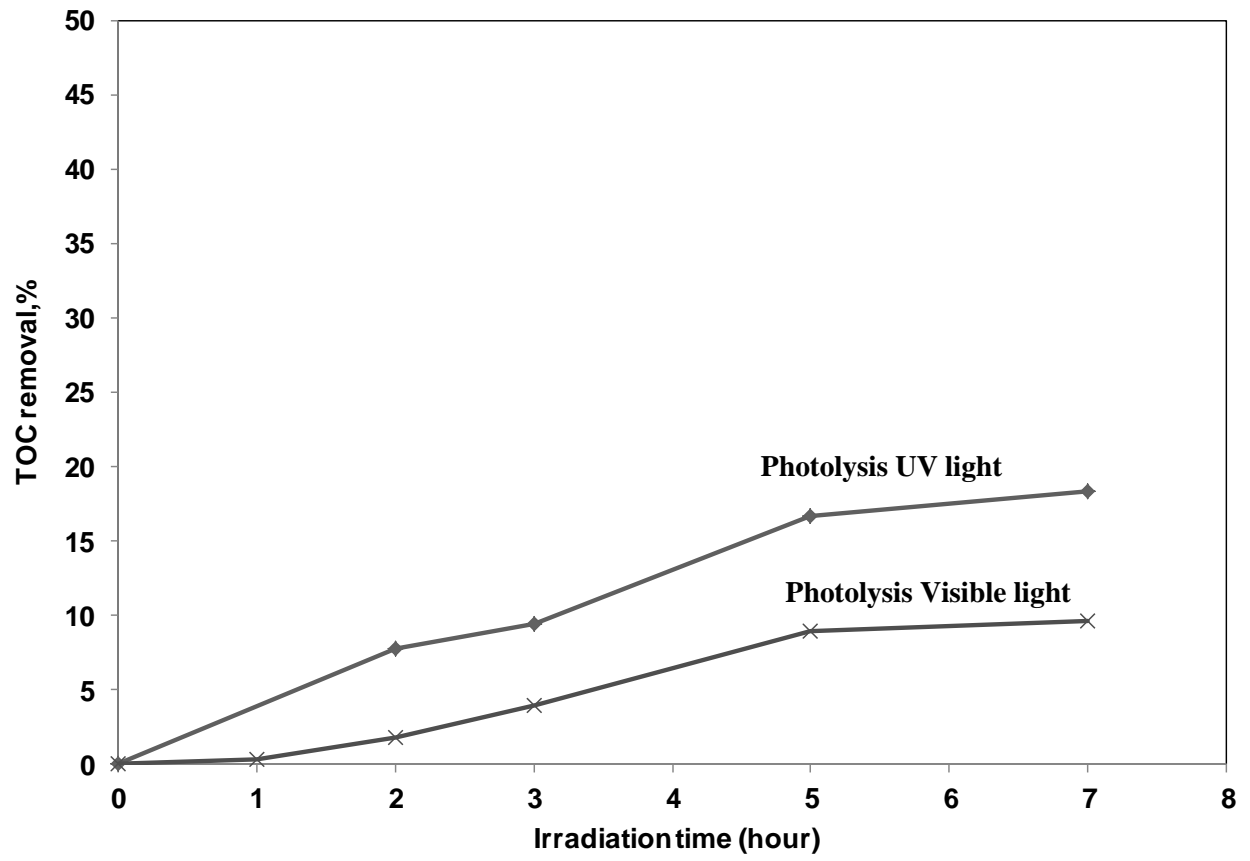
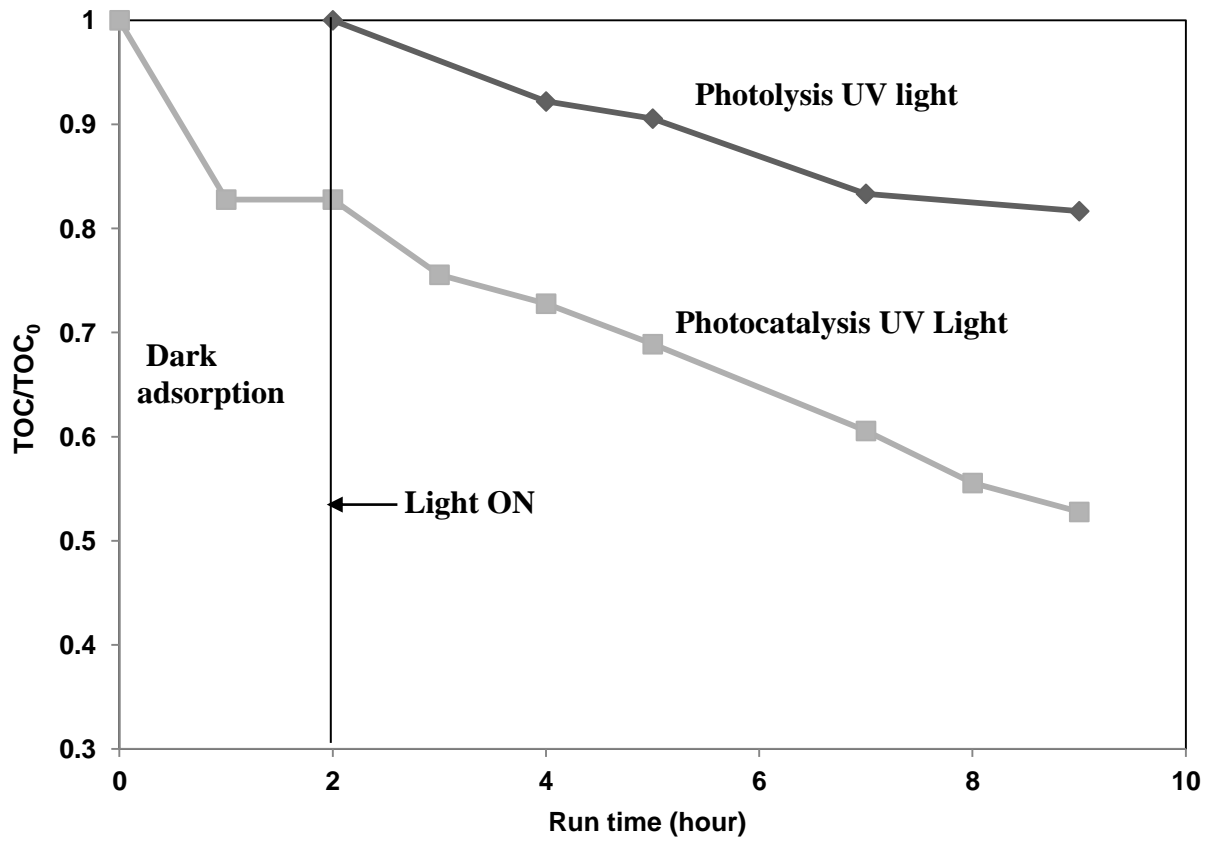


Figure 3 Comparison between photolysis under visible light and UV light



Figure4



**Figure 4** Comparison between photolysis and photocatalysis (Nt dosage: 3g/L) using UV light sources

Figure5

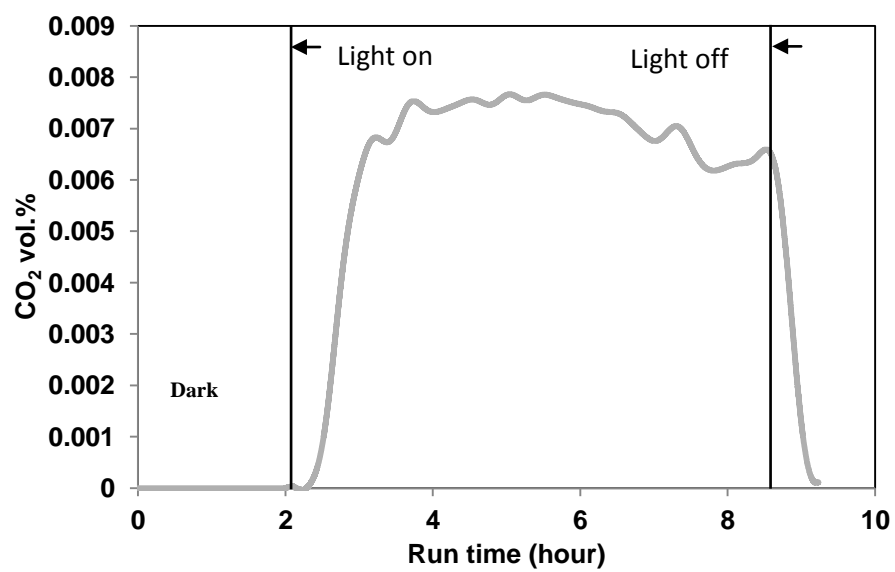
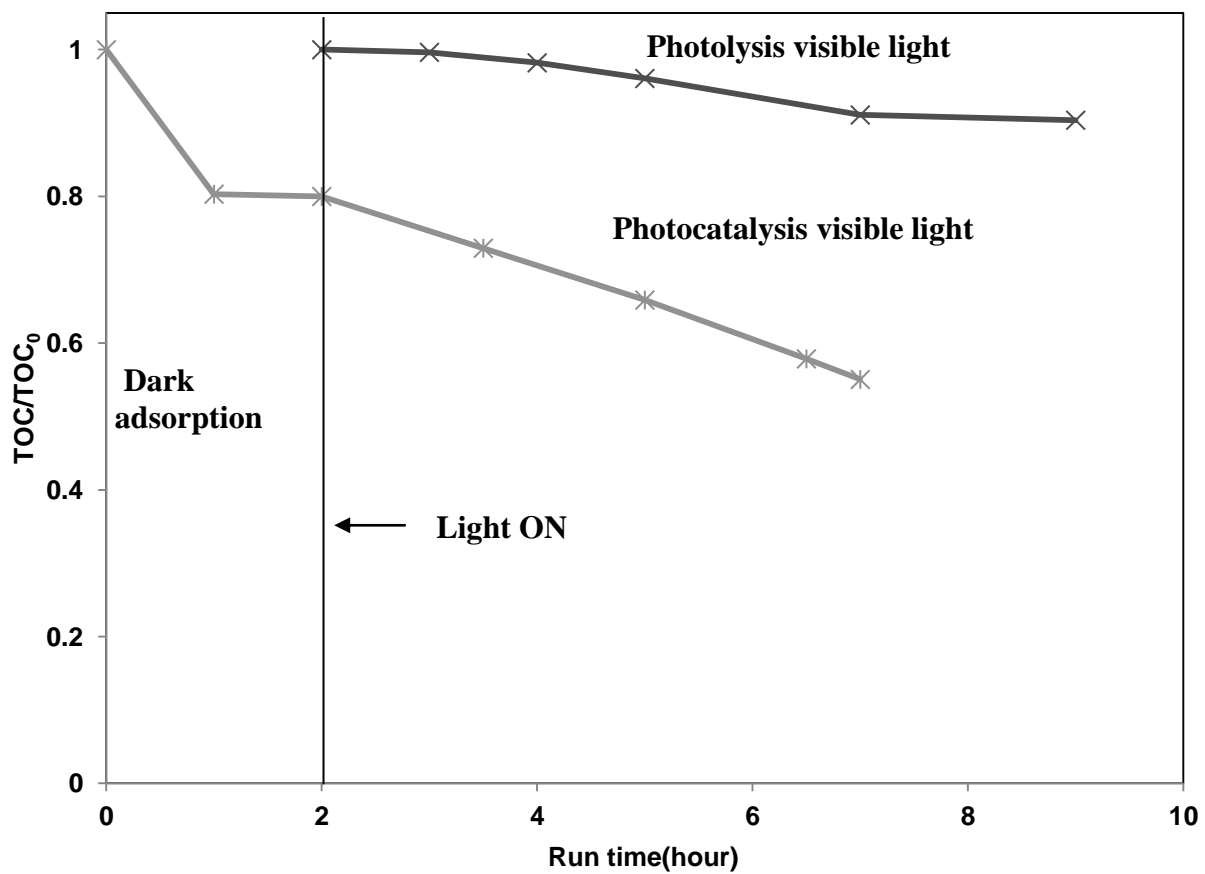


Figure 5 Gas phase analysis during photocatalysis in presence of UV irradiation.

Figure6



**Figure 6** Comparison between photolysis and photocatalysis (Nt dosage : 3g/L) using visible light ( blue LEDs )sources

Figure7

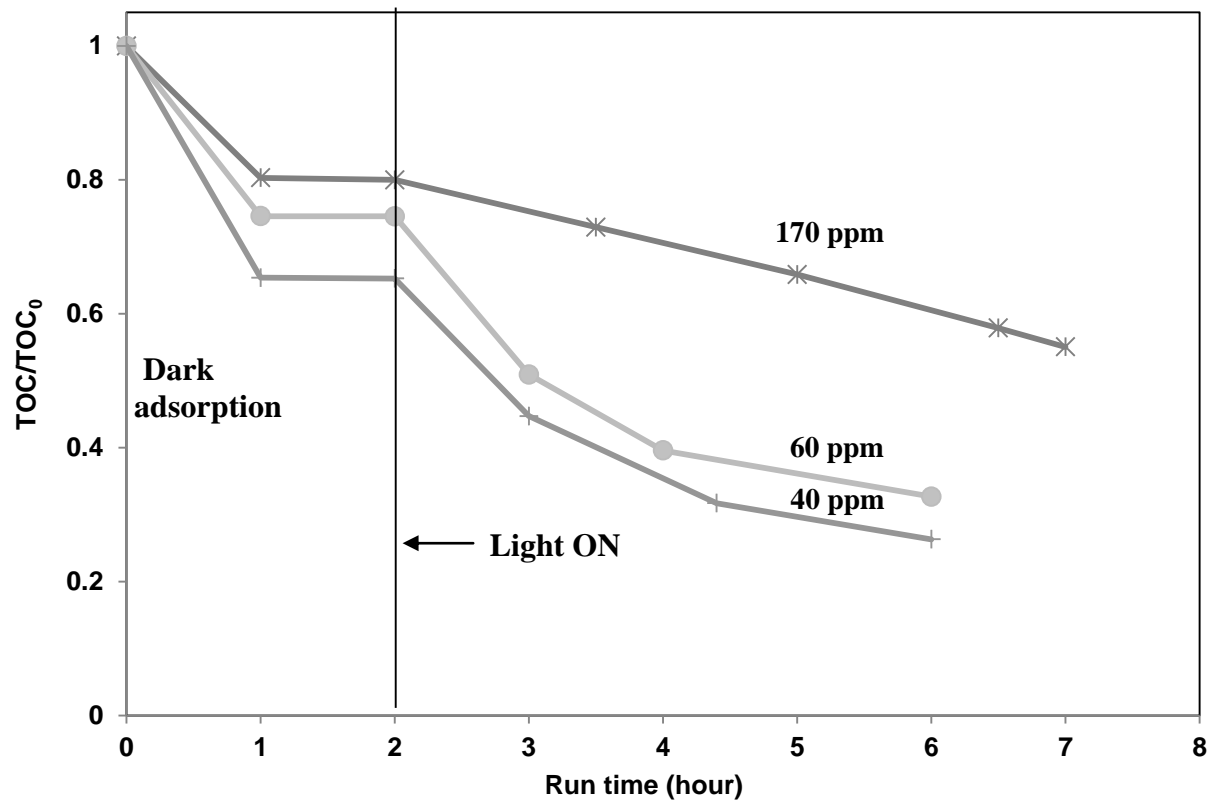


Figure 7 Evaluation of SP mineralization under visible light with different initial TOC<sub>0</sub>.

Figure8

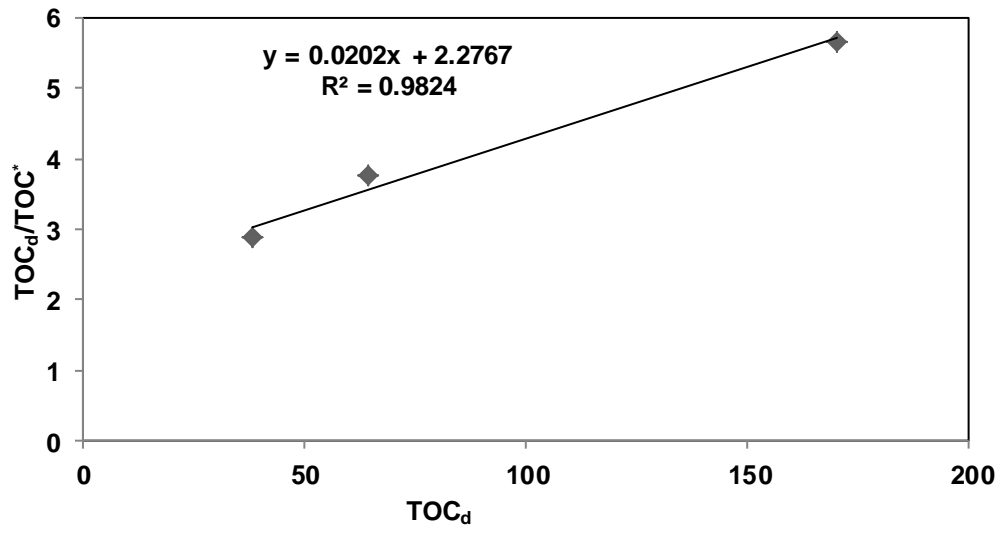
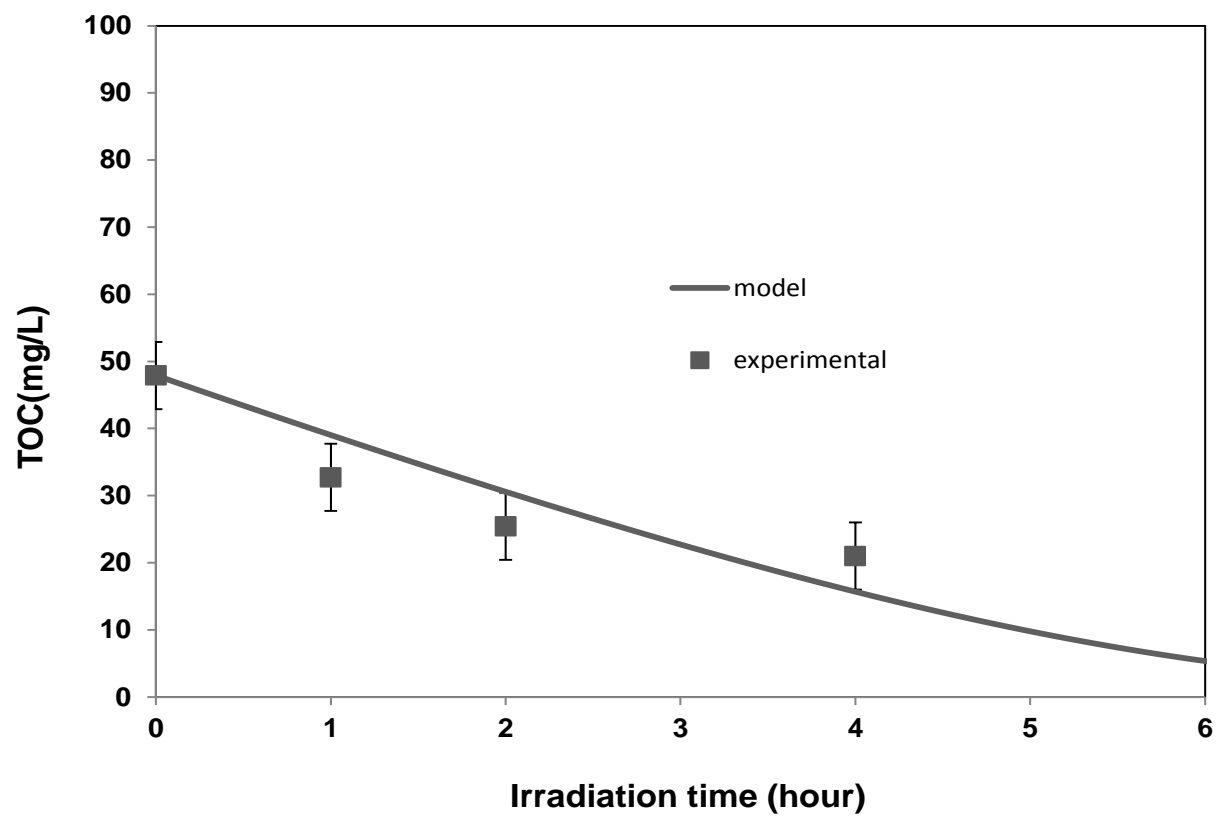


Figure 8 Evaluation of SP adsorption constant

Figure9



**Figure 9** Comparison between model calculation and experimental data to find the reaction constant

Figure10

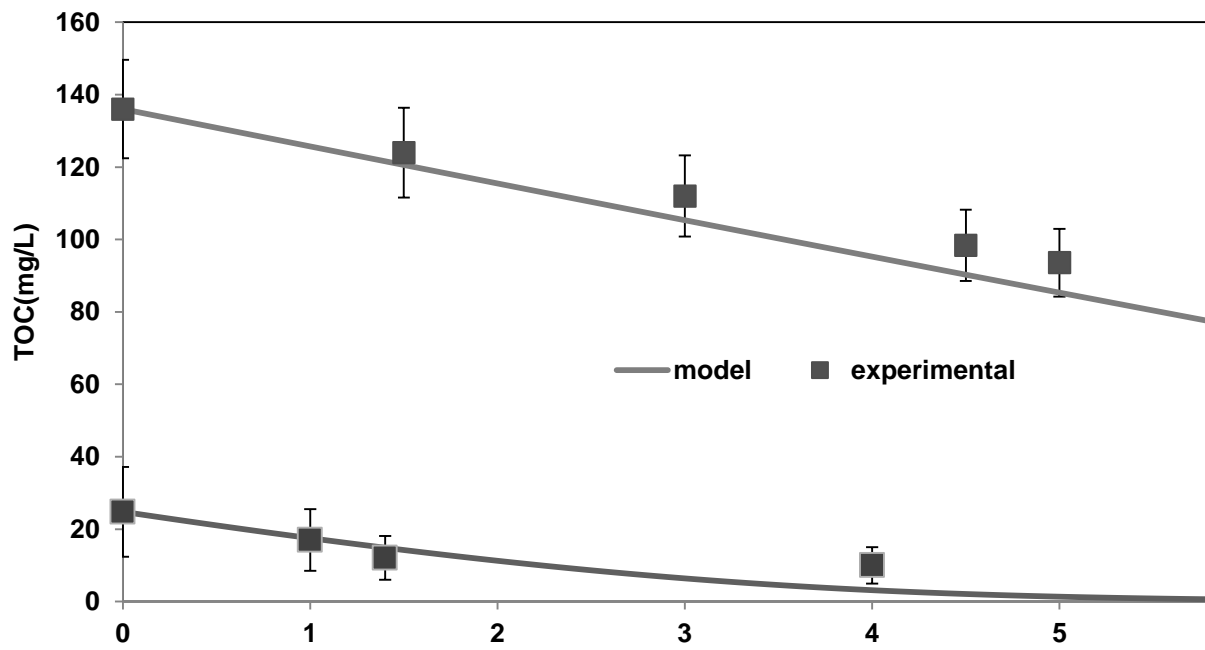


Figure 10 Experimental and predicted data as a function of initial TOC<sub>0</sub>

Figure11

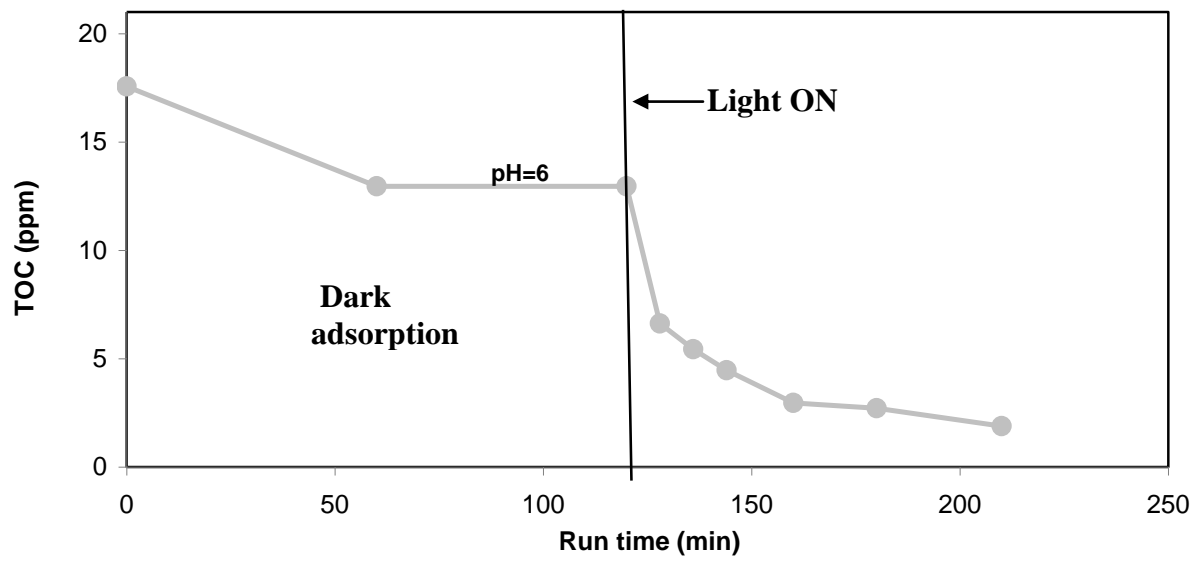


Figure 11 Photocatalytic results on the real pharmaceutical wastewater using blue LEDs light